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DEPENDENCE OF THE CAPACITY RATIO ON THE COMPOSITION OF THE BINARY MOBILE PHASE IN LIOUID-SOLID ADSORPTION CHRO-NT BRANK STOLEN MATOGRAPHY

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(First received November 29th, 1977; revised manuscript received February 15th, 1978) where the mean of the set of the set of the set of the set. I have been also have been also have been also have

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The dependence of the capacity ratio on the composition of the binary mobile phase is discussed in terms of Snyder's treatment. The relationships obtained for the capacity ratio have been tested on experimental data. The derivation of the relationship for the capacity ratio discussed by Jandera and Churacek has been examined.

INTRODUCTION

Increasing interest in gradient elution chromatography as a rapid method of analysis has made desirable the eluadation of the theoretical basis of the process of liquid-solid adsorption chromatography. The basic problems involved are optimization of the time of analysis and the resolution. One of the main parameters that determines the process of elution is the capacity ratio. Although in isocratic elution at an infinitely low concentration of the sample the capacity ratio remains constant for a given chromatographic system, in gradient elution it is necessary to know the relationship between the capacity ratio, k_{AB} , and the composition of the mobile phase A-B.

It follows from many papers¹⁻⁸ that three types of relationships describing the dependence between the capacity ratio and the concentration of the component that is the more efficient eluent in a binary mobile phase can be distinguished:

$$\log k'_{\rm AB} = a + b \log x_{\rm B} \tag{1a}$$

 $\log k'_{AB} = a + b x_{B}$

 $1/k'_{AB} = a + b x_{B}$ (1c)

(16)

where $x_{\rm B}$ is the molar fraction (or concentration) of the more efficient eluent B in the binary mobile phase A-B and a and b are constants. Numerous studies^{5.7,9} have shown that these three relationships can be used to characterize a chromatographic system したがないないであり、そうでは、そうであるのです。 1993年に、1995年に、そうでは、1995年に、1995年には、1995年には、1995年には、1995年に、1995年に、1995年に、1995年には、1995年に、1995年に、1995年に、1995年に、1995

DISCUSSION OF THE JANDERA-CHURACEK DERIVATION OF THE RELATIONSHIP
BETWEEN LOG
$$k_{AB}$$
 AND LOG x_{B}

Jandera and Churacek⁷ derived eqns. Ia and 1b; the former was obtained on the basis of Snyder's theory of liquid-solid adsorption chromatography¹⁰. Their derivation of eqn. la requires further comment. According to their derivation, the constants a and b are expressed by $a = \log k_{\rm B}$ and $b = -n = -\omega_{\rm S}/\omega_{\rm B}$, where $k_{\rm B}$ is the capacity ratio for a sample compound S in pure solvent B and ω_s and ω_{s} are the molecular areas occupied by molecules of sample S and solvent B, respectively.

Let us discuss the constants a and b according to Snyder's treatment¹⁰. Snyder obtained the following expression:

$$\varepsilon_{AB} = \varepsilon_A + (\alpha \omega)^{-1} \log \left[x_B \, 10^{-\alpha \omega (\varepsilon_A - \varepsilon_B)} + 1 - x_B \right] \tag{2}$$

for the strength ε_{AB} of a binary solvent A-B, assuming the following:

(a) an expression for equilibrium constant, K, defining the following reaction:

 $B_{(\text{liquid phase})} + A_{(\text{solid phase})} \rightleftharpoons B_{(\text{solid phase})} + A_{(\text{liquid phase})}$

$$K = 10^{a\omega(e_{\rm B}-e_{\rm A})} = \frac{y_{\rm B}(1-x_{\rm B})}{(1-y_{\rm B})x_{\rm B}}$$
(3)

(b) a relationship between the capacity ratios k'_{AB} and k'_{B} :

$$\log\left(k'_{AB}/k'_{A}\right) = \alpha \,\omega\left(\varepsilon_{A} - \varepsilon_{AB}\right) \tag{4a}$$

 $\log \left(k_{\rm p}^{\prime} / k_{\rm A}^{\prime} \right) = \alpha \, \omega \left(\varepsilon_{\rm A} - \varepsilon_{\rm B} \right)$ (4b)

(c) additivity of the capacity ratios k'_{A} and k'_{B} :

$$k'_{AB} = y_B k'_B + (1 - y_B) k'_A$$
(5)

(d) equality of the molecular areas occupied by molecules of adsorbed samples, solvents A and B:

$$\omega_{\mathbf{A}} = \omega_{\mathbf{B}} = \omega_{\mathbf{S}} = \omega \tag{6}$$

In the above equations, k_A denotes the capacity ratio for a sample compound in pure solvent A; α is the surface activity function; ε_A and ε_B denote the strengths of the solvents A and B, respectively; and y_{B} is the molar fraction of solvent B in the surface phase. Jandera and Churacek, again introducing eqn. 2 into eqn. 4a but this time omitting Snyder's assumption about the equality of the molecular areas of

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the sample compound S and the more efficient eluent B, as well as neglecting the term $1 - x_B$ in eqn. 2, obtained eqn. 1a. A direct consequence of neglecting the term $1 - x_B$ is an irregular behaviour of eqn. 1a in the region of infinitely low concentrations of x_B . In real systems, it would be expected that k'_{AB} will tend towards k'_A at $x_B \rightarrow 0$, whereas eqn. 1a gives $k'_{AB} \rightarrow \infty$ within this limit. Eqn. 1a also suggests that k_{AB} for any sample component chromatographed does not depend on the properties of the less efficient eluent A in the binary solvent mixture A-B. Hence, it can be concluded that for a less efficient eluent in the binary mobile phase, k'_{AB} will be constant at a given concentration of the more efficient eluent B. However, numerous experimental data show that k'_{AB} at a given concentration x_B is dependent on the properties of all components of the mobile phase. The treatment of Jandera and Churacek resulted in a value of $n \neq 1$, which is due to the incorrect application of eqn. 6. Although the values of n in eqn. 1a may be different from unity, which is often confirmed experimentally, the correct application of Snyder's assumption leads to the value n = 1.

DERIVATION OF THE DEPENDENCE OF THE CAPACITY RATIO IN TERMS OF SNYDER'S THEORY

In the light of the above discussion, it seems appropriate to derive a relationship between the capacity ratio, k'_{AB} , and the composition of the binary mobile phase in which the parameters depend on the properties of both the solvents of the mobile phase and the sample being chromatographed. Moreover, this relationship should be correct for the whole range of concentrations x_B . Such a relationship can be obtained by using Snyder's assumptions (a)-(d) above. Combining eqn. 4b with eqn. 3, we obtain

$$k'_{\rm A}/k'_{\rm B} = \frac{y_{\rm B}(1-x_{\rm B})}{(1-y_{\rm B})x_{\rm B}}$$
(7)

Then, elimination of the variable y_B from eqns. 5 and 7 leads to

$$\frac{1}{k'_{AB}} = \frac{1}{k'_{A}} + \left(\frac{1}{k'_{B}} - \frac{1}{k'_{A}}\right) x_{B}$$
(8)

This equation is related to the empirical relationship in eqn. 1c. Of course, eqn. 8, assuming $1 - x_B \ll Kx_B$, gives

$$\log k'_{AB} = \log k'_{B} - \log x_{B} \tag{9}$$

which corresponds to the special case of the empirical relationship in eqn. 1a, *i.e.*,

$$\log k'_{\rm AB} = a - \log x_{\rm B} \tag{10}$$

with -b = n = 1. It can easily be seen that eqn. 8 predicts correctly the values of k_{AB} at the limiting concentrations of x_B ($x_B = 0$ and $x_B = 1$) and is a direct consequence of Snyder's theory¹⁰, *i.e.*, this equation is obtained from Snyder's theory

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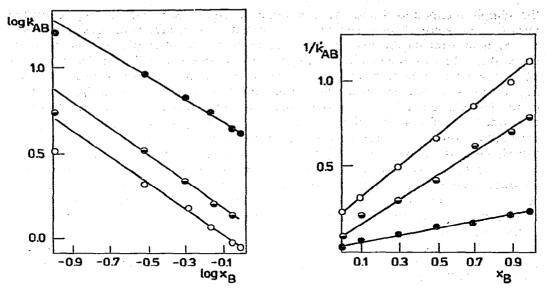


Fig. 1. Linear dependences plotted according to eqn. 1a. (a) $A = C_6H_6$, $B = C_6H_{12}O_6$, S = 2-amino-3-methylpyridine, stationary phase = alumina; (O) $A = CCl_4$, $B = CHCl_3$, S = 2,6-dimethylquinoline, stationary phase = alumina; (a) $A = CCl_4$, $B = CHCl_3$, S = quinoline, stationary phase = silica gel.

Fig. 2. Linear dependences plotted according to eqn. 8. Symbols as in Fig. 1.

without any further simplifications. Eqn. 8 has also been discussed by Soczewiński⁹ and Scott and Kucera⁸ by using other theoretical approaches.

In Figs. 1 and 2 the agreement of eqns. 1a and 8 with the experimental data obtained by Ościk and Chojnacka¹¹ and Rózyło¹² is compared. It can be seen that both equations describe the experimental data at higher values of x_B , but at low concentrations of solvent B eqn. 8 gives considerably better results. These results confirm the theoretical discussion concerning the regions of applicability of eqns. 1a and 8. It is interesting, however, that eqn. 1a agrees very well with the experimental data at higher values of x_B for adsorption systems with $n \neq 1$. This agreement is not covered by the Snyder's treatment based upon assumptions (a)-(d); however, if A and B have very different molecular sizes, changes must be made to assumptions (a) and (d), which leads to a more general relationship for k'_{AB} .

A more generalized form of reaction in (a) can be written as

 $B_{(\text{liquid phase})} + mA_{(\text{solid phase})} \rightleftharpoons B_{(\text{solid phase})} + mA_{(\text{liquid phase})}$

where $m = \omega_{\rm B}/\omega_{\rm A}$. This leads to the following expression for the equilibrium constant:

$$K = \frac{(1 - x_{\rm B})^m y_{\rm B}}{x_{\rm B} (1 - y_{\rm B})^m}$$
(11)

when $m \neq 1$, eqn. 8 cannot be solved analytically with respect to $y_{\rm B}$, and only numerical solutions are available which are not convenient for gradient optimization.

However, in the special case when y_B approaches unity and K is sufficiently large (a large difference in concentration between the two components of the mobile phase), from eqns. 8 and 5 the following expression can be obtained:

$$\log k'_{AB} = \log \left(k'_{A} / \overline{K^{m}} \right) - \frac{1}{m} \log x_{B}$$
(12)

for high x_B values. This equation is formally analogous to eqn. 1a where $-1/m = b \neq -1$ (or $n \neq 1$). Thus, in conclusion, it can be stated that on the basis of Snyder's theory, full mathematical justification has been found for eqn. 8, and this theory leads to the approximate eqns. 9 (b = -1) and 12 ($b \neq -1$).

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